

## Biodegradable Polymer

This invention relates to improvements in biodegradable polymeric products particularly starch based polymers.

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### Background to the invention

There is an increasing demand for many plastic products used in packaging to be biodegradable. Trays in biscuit and chocolate packages are one example.

Starch films have been proposed as biodegradable alternatives for some time.

10 USA patent 3949145 proposed a starch/polyvinyl alcohol/glycerol composition for use as a biodegradable agricultural mulch sheet.

Difficulties have been encountered in producing starch based polymers particularly by hot melt extrusion. The molecular structure of the starch is adversely affected by the shear stresses and temperature conditions needed to plasticise the starch  
15 and pass it through the extrusion die. For most products foaming has to be avoided and this generally requires attention because of the water content of the starch. Foaming has been avoided by degassing the melt prior to exiting the die as suggested in USA patents 5314754 and 5316578. The latter patent also avoids adding water to the starch. As explained in USA patent 5569692 by not drying  
20 starch and avoiding the addition of water the starch can be processed at temperatures between 120°C and 170 °C because the water bound to the starch does not generate a vapour pressure such as to require high pressures.

Another approach to improving the melt processability of starch is to provide an additive as in USA patent 5362777 which reduces the melting point of the starch.

25 The additive is selected from dimethyl sulfoxide, a selection of polyols and amino or amide compounds.

In order to produce starch polymers for particular applications they have been blended with a range of other polymers. Biodegradable blown films are disclosed in USA patent 5322866 which blends raw starch, polyvinyl alcohol and talc with  
30 glycerol and water. USA patent 5449708 discloses compositions of starch ethylene acrylic acid and a salt of stearic acid plus a glycerol based lubricant. Flexible and clear transparent sheets are disclosed in USA patent 5374304. These are composed of a high amylose starch and a glycerol plasticizer. The use of starch in

conjunction with high amylose or modified starches has also been proposed. USA patents 5314754, and 5316578 both suggest the use of modified starches including hydroxypropyl substituted starches. Hydroxypropylation reportedly increases elongation at break and burst strength and improved resilience in the polymers. Although the efficacy of these special and modified starches is recognised, their cost inhibits the commercial acceptability of the products made from them.

It is an object of this invention to provide a biodegradable polymer which can be processed and thermoformed into sheet and shaped products without difficulty and have acceptable properties for its intended uses.

### Brief Description of the Invention

To this end the present invention provides a process for forming biodegradable polymers which includes the steps of

- a) forming a mixture of starch, a modified starch, a water soluble polymer or copolymer containing vinyl alcohol units, up to 20 % of added water or a polyol plasticizer and 0.4 to 1.5 % by weight of a C<sub>12-22</sub> fatty acid or salt,
- b) working the mixture and forming a melt within the temperature range of 130°C to 160 °C
- c) reducing the temperature and further working the mixture and the extruding the mixture or injecting the mixture into a mould at a temperature of 85 °C to 105 °C without the need to remove water.

The process as defined allows starch based mixtures to be extruded without foaming. The need to vent the extruder to remove water prior to the mix exiting the extrusion die is not needed. Both rigid sheet and flexible starch based films can be made using this process. The foaming temperature of the mix is raised above the temperature at which the melt is most easily plasticised and extruded.

In another aspect, the present invention provides a biodegradable polymer having the composition

- a) from 8 to 80% by weight of a starch modified to include an  
5 hydroxyalkyl  $C_{2-6}$  group or modified by reaction with an anhydride of a dicarboxylic acid
- b) from 0 to 87.9% of starch
- c) from 4 to 11% by weight of a water soluble polymer selected from  
polyvinylacetate, polyvinyl alcohol and copolymers of ethylene and vinylalcohol  
10 which have a melting point compatible with the molten state of the starch components
- d) from 0 to 20% by weight of a polyol plasticiser
- e) from 0.1 to 1.5 % by weight of a  $C_{12-22}$  fatty acid or salt and
- f) from 0 to 12 % by weight of added water.

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The compositions defined include formulations suitable for forming films or thermoforming rigid products such as packaging trays. The defined compositions are easier to process as they can be extruded in film or sheet form without foaming. The extruded sheet can be thermoformed into shaped trays or containers  
20 for use as biodegradable packaging. Usually the need to vent the extruder to remove water prior to the mix exiting the extrusion die is not needed with these formulations.

The upper limit to the content of the modified starch is determined by its cost. This component contributes structural benefits to the resulting material. A preferred  
25 component is hydroxypropylated amylose. Other substituents can be hydroxyethyl or hydroxybutyl to form hydroxyether substitutions, or anhydrides such as maleic phthalic or octenyl succinic anhydride can be used to produce ester derivatives. The degree of substitution[ the average number of hydroxyl groups in a unit that are substituted] is preferably 0.05 to 2. The preferred starch is a high amylose  
30 maize starch. A preferred component is a hydroxypropylated high amylose starch A939 marketed by Goodman Fielder. A preferred concentration range to meet cost parameters for biscuit trays is 12 to 24 %.

The other starch component is any commercially available starch. This may be derived from wheat, maize, potato, rice, oat, arrowroot, and pea sources.

Generally the water content is about 10 to 15 %. A preferred concentration range for starch is 50 to 70.6%

The polymer component c) of the composition is preferably compatible with starch, water soluble, biodegradable and has a low melting point compatible with the processing temperatures for starch. Polyvinyl alcohol is the preferred polymer but polymers of ethylene-vinyl alcohol, ethylene vinyl acetate or blends with polyvinyl alcohol may be used. A preferred concentration range for sheet material is 7 to 9%.

The preferred plasticiser is glycerol although ethylene glycol and diethylene glycol are also suitable as is sorbitol. Cost and food contact are important issues in choosing the appropriate plasticizer. For low humidity environments such as biscuit packages it has been found that lower plasticizer content improves the toughness and long term resilience of the material. This is partly due to the properties of the starch ether component and the fact that at low humidity plasticizers such as glycerol tend to remove water from the starch polymer and make it more brittle. It is possible to process the formulation with no plasticizer and the rigid polymer formed is flexible and has good impact resistance at low humidity. When the plasticiser content is low additional water is added to improve processing. Thus the plasticizer content is preferably 0 to 12% and the water content is 12 to 0%. For film processing the plasticizer content is preferably higher than for rigid sheet products. Higher concentrations of plasticiser improve flexibility and for flexible packaging films or mulch films the preferred plasticiser content is 10 to 16%.

The fatty acid or fatty acid salt component is preferably present in concentrations of 0.6 to 1%. Stearic acid is the preferred component. Sodium and potassium salts of stearic acid can also be used. Again cost can be a factor in the choice of this component but lauric, myristic, palmitic, linoleic and behenic acids are all suitable. It is found that the acid tends to accumulate near to the surface of the composition as it is extruded.

### **Detailed description of the invention**

Processing conditions depend on the formulations and the desired properties of the product to be produced. The materials need to be heated above 140 °C in the

extruder to fully gelatinise the starches. The die temperature needs to be controlled below 110°C to avoid foaming.

The preferred method of carrying out this invention involves mixing the starch, modified starch, vinylalcohol polymer lubricant and fatty acid components into a free flowing powder. The premixing can be carried out in any conventional mixer. The powder is then introduced into a screw extruder and subjected to an elevated temperature by the shearing action of the screw and the application of external heat to the barrel. The temperature is raised to a maximum in the range of 130°C to 160°C. Any liquid components including additional water are introduced during this initial phase. The melt that is formed is then propelled toward the die and in moving forward the temperature is reduced to a value in the range of 85 °C to 105°C.

A typical extrusion for rigid products has the following parameters:

Temperature profile °C : 60, 70, 90, 110, 130, 145, 130, 120, 110

Screw Speed 120 rpm

Die Pressure 1400 psi

Flexible film can be formed by simply extruding from a sheet forming die and then increasing the speed of the take-off roller to achieve the reduced thickness needed for flexible film. Cooling of the film between the die and the roller is usually needed to ensure that the film does not adhere to the roller. De-humidified air to cool the film also assists in removing excess moisture from the film surface. If the film is formed by the blown tube method dehumidified air is used to blow the film as it exits the die. Talc may also be entrained in the air stream to reduce blocking of the film.

#### Examples 1-14

Biscuit trays were made by extruding a sheet and subsequently thermo forming the tray in a hot press. A twin screw extruder was used with a screw speed of 130rpm. The barrel temperature profile was 95 [die], 95 [adapter], 95, 95, 95, 95, 100, 130, 140, 150, 140, 110, 90, 60. The process avoided foaming at the die and did not require venting of the barrel to remove moisture.

The formulations and the initial observations of the trays' performance are given in the table 1.

More detailed tests were carried out on sheets made from examples 9 to 14 and these results are shown in tables 2, 3 & 4.

**TABLE 1**

Example	A939 [hydroxy propylated amylose]	Wheat Starch	PVOH	Glycerol	Stearic Acid	Remarks
1	37.46	37.46	8.1	14.29	0.84	Includes 4.02% talc no foam, fairly flexible, very strong
2	33.51	33.51	7.46	21.05	0.75	Includes 3.72% CaCO <sub>3</sub> No foam, flexible, weak
3	34.42	34.42	7.66	18.92	0.77	Includes 3.81% CaCO <sub>3</sub> slight foam, flexible, strong
4	35.38	35.38	7.88	16.67	0.79	Includes 3.92% CaCO <sub>3</sub> slight foam, flexible, strong
5	37.34	37.34	7.87	16.67	0.78	no foam, flexible, strong
6	38.41	38.41	8.08	14.29	0.81	no foam, flexible, strong
7	39.71	39.71	8.03	11.76	0.79	no foam, flexible, very strong
8	38.03	38.03	7.69	11.27	0.76	Includes 4.23% water no foam, flexible, fairly strong
9	81	0	8	10.2	0.8	
10	65	16	8	10.2	0.8	
11	57	24	8	10.2	0.8	
12	24	57	8	10.2	0.8	
13	16	65	8	10.2	0.8	
14	0	81	8	10.2	0.8	

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**Table 2 - Youngs Modulus**

example	initial	24 hours	1 week
9	942.591	355.992	395.783
10	743.174	611.025	459.516
11	729.490	578.648	567.977
12	905.406	609.926	600.324
13	1079.915	519.888	688.400
14	1155.357	797.400	749.335

**Table 3 – Stress at 0.2% yield offset**

C	initial	24 hours	1 week
9	9.522	2.189	3.413
10	6.016	4.144	3.078
11	7.313	3.823	4.102
12	7.929	3.814	5.695
13	12.624	5.178	6.263
14	14.175	6.884	6.565

**Table 4 - % strain at the breaking point**

C	initial	24 hours	1 week
9	56.969	82.532	78.304
10	49.845	43.613	41.588
11	56.550	56.166	37.591
12	19.188	47.033	21.798
13	17.699	40.952	21.165
14	8.552	27.661	16.145

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From the above tests and examples and based on cost considerations a suitable formulation for this biscuit tray application is:

A939 [hydroxy propylated amylose]	Wheat Starch	PVOH	Glycerol	Stearic Acid
15	65.2	8	11	0.8

- 10 The trays are biodegradable and have strength and flexibility properties comparable to the non biodegradable materials currently used. The costs of production are also comparable.

**Examples 15 - 22**

The effect of stearic acid content on the composition was tested using a formulation of :

	Wheat starch	36%
5	Modified Amylose A939	36%
	Polyvinyl alcohol	8%
	Glycerol	10%
	Water	10%

- 10 The mixture was processed at a feed rate of 1.5 a screw speed of 100 rpm and the temperature profile was 70, 90, 100, 130, 140, 140, 130, 115, 110, 110, 110[die]

Example	Stearic acid content [%]	Torque [%]	Mass [g/min]	Quality of Sheet [observation]
15	0.0	57	101	Rough surface
16	0.4	51	100	Nice sheet
17	0.8	44	106	Nice sheet
18	1.2	39	114	Nice sheet
19	2	38	106	Sheet with some holes
20	3	38	106	Sheet with holes
21	4	35	101	Sheet with a lot of holes
22	5	34	102	Sheet with a lot of holes

The results show that torque is decreased with increase in stearic acid content.

- 15 Output mass peaks at a stearic acid content of 1.2 g. the preferred range of stearic acid is 0.4 to 1.5 %.



**Examples 23-26**

The following four formulations have also been found suitable for use in forming packaging trays for foodstuffs such as chocolates and biscuits.

Materials	Example 23	Example 24	Example 25	Example 26
A939	39.5	39.5	79	79
Wheat starch	39.5	39.5	0	0
PVOH	8	8	8	8
Stearic acid	1	1	1	1
Glycerol	6	3	6	3
Water	8	10	8	10

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**EXAMPLE 27**

Formulations as shown in table 5 were prepared for the purpose of assessing their performance under low and high humidity conditions and to assess the

10 performance of the plasticiser under these conditions.

**Table 5**

Materials	A939 %	PVOH %	Stearic acid %	Water %	Glycerol %
A	79.5	7.95	0.8	0	11.75
B	78.31	7.84	0.8	4.35	8.7
C	78.31	7.84	0.8	7.25	5.8
D	78.31	7.84	0.8	10.15	2.9
E	79.5	7.95	0.8	11.75	0

Table 6 shows the strength characteristics at 65% RH and table 7 shows the

15 characteristics at 15% RH for these formulations.

**Table 6 – 65%RH**

Formulation	Modulus [Mpa]	Yield S. [Mpa]	Elongation %
A	547	3.2	118
B	774	7.1	78
C	1080	14	65
D	1556	18	40
E	1832	27	28

**5 Table 7 – 15%RH**

Formulation	Modulus [Mpa]	Yield S. [Mpa]	Elongation %
A	1750	27	20
B	1916	33	26
C	2035	33	23
D	2447	38	24
E	2696	41	23

Tables 6 and 7 show that under high or medium relative humidity Glycerol improves toughness as measured by elongation. Under low relative humidity the glycerol absorbs water from the starch in the polymer and this decreases toughness.

**Example 28**

Two formulations were prepared on being formula E of example 27 and the other being the same except that 50 % of the A939 was replaced by wheat starch. Both formulas were processed extruded as sheet and then thermoformed into biscuit trays. The trays were used in a product trial where biscuits were placed in the tray packaged and then stored for three months. The performance and appearance of the trays were acceptable and as good as conventional non – biodegradable trays. The significant advantage of the trays made by both formulations were that disposal was much simpler. Conventional trays are difficult for consumers to

compress and their volume cannot be significantly reduced but by simply running these trays under a tap they can be compressed by hand into a small disposable pellet.

- 5 From the above description and examples it can be seen that the present invention provides a biodegradable starch polymer that is comparable in price and performance characteristics to conventional non-biodegradable polymers. Consequently packaging of products such as biscuits and chocolates using a rigid thermoformed tray can be just as presentable and attractive with the added benefit
- 10 of being environmentally friendly. Similarly packaging of products such as bread, in flexible packaging films, can also be attractive and biodegradable.